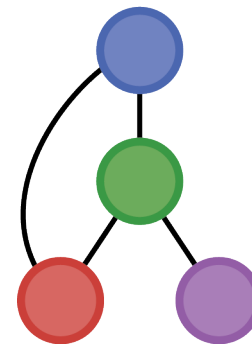


Optimization Abstraction Layer for Acausal/Equation-Oriented Models in Julia

Dimitri Alston, Joseph Choi, Pengfei Xu
Matthew Stuber, P&W Associate Professor in
Advanced Systems Engineering

November 5th, 2025

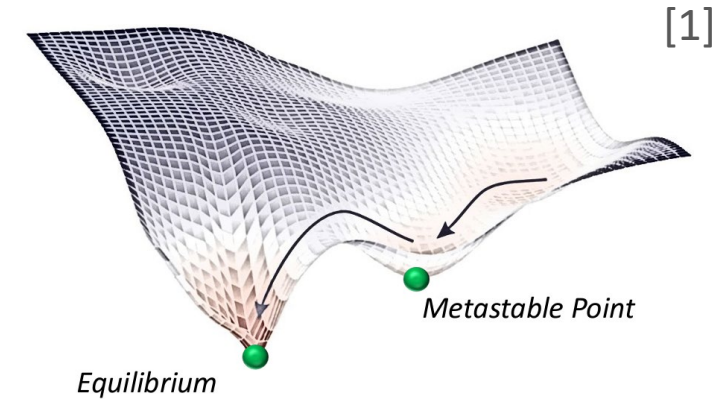
2025 / AICHE
ANNUAL
MEETING



Process Systems and
Operations Research
Laboratory

Global Optimization

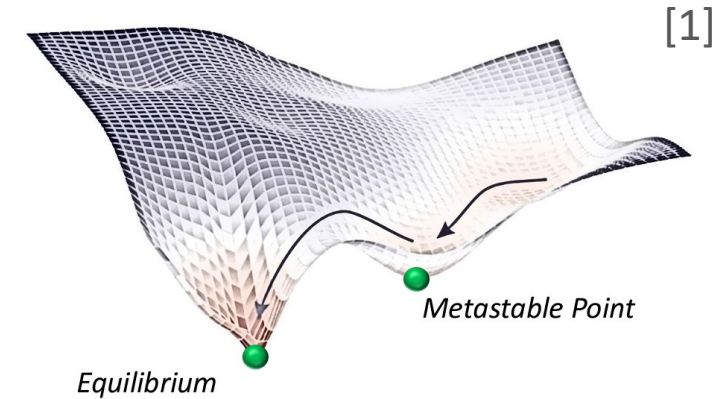
- Nonconvex problems arise in many applications
 - Thermodynamic stability
 - Kinetic parameter estimation
 - Design under uncertainty



[1] Grajcarova, L. Simulations of structural phase transitions in crystals using ab initio metadynamics. INIS-IAEA. (2013).

Global Optimization

- Nonconvex problems arise in many applications
 - Thermodynamic stability
 - Kinetic parameter estimation
 - Design under uncertainty
- Dynamic optimization problems



$$\min_{\mathbf{p} \in P} \phi(\mathbf{x}(\mathbf{p}, t_f), \mathbf{p})$$

$$\text{s.t. } \dot{\mathbf{x}}(\mathbf{p}, t) = \mathbf{f}(\mathbf{x}(\mathbf{p}, t), \mathbf{p}, t) = \mathbf{0} \quad \forall t \in I = [t_0, t_f]$$

$$\mathbf{x}(\mathbf{p}, t_0) = \mathbf{x}_0(\mathbf{p})$$

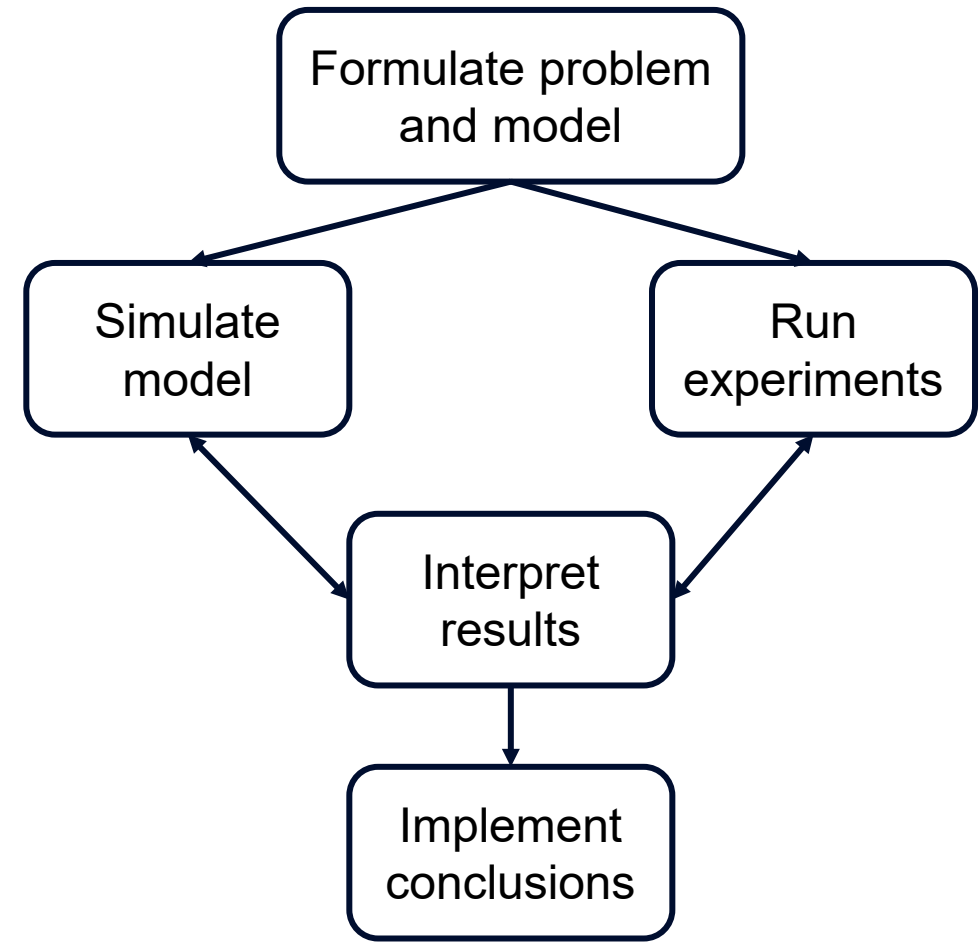
$$\mathbf{g}(\mathbf{x}(\mathbf{p}, t), \mathbf{p}) \leq \mathbf{0}$$

$$P = \{\mathbf{p} \in \mathbb{R}^m : \mathbf{p}^L \leq \mathbf{p} \leq \mathbf{p}^U\}$$

[1] Grajcarova, L. Simulations of structural phase transitions in crystals using ab initio metadynamics. INIS-IAEA. (2013).

Modeling and Simulation

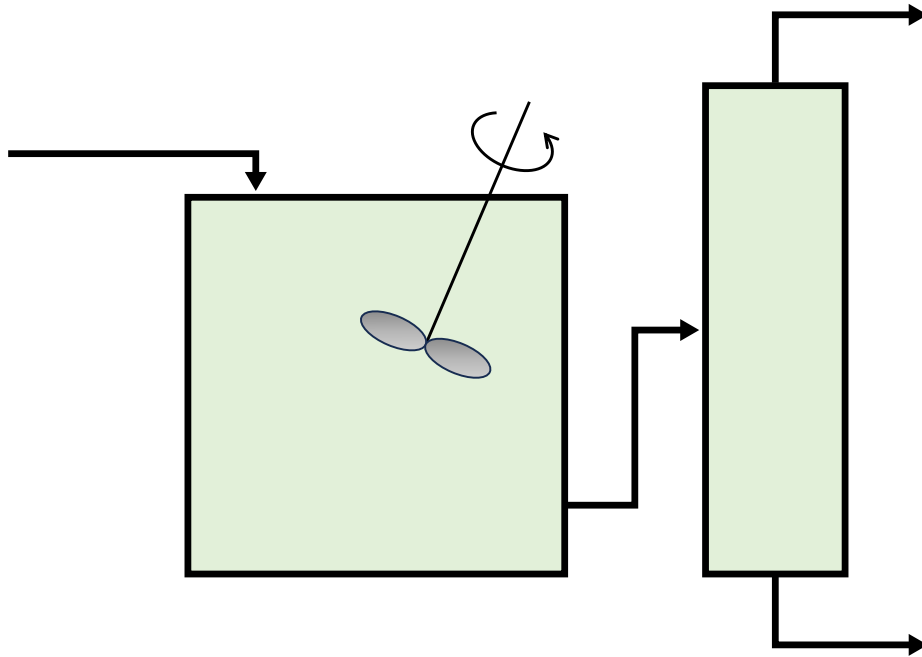
- Applicable in various contexts
 - Proof-of-concept
 - Modification
 - Comparison
 - Optimization
- Eliminate costs of real-world experiments
- Provide support at all stages of design



Modeling and Simulation Approaches

Causal/Sequential-Modular

Acausal/Equation-Oriented



$$y_{2,A} + y_{2,B} + y_{2,C} = 1$$

$$y_{2,B}F = y_{1,B} + Vr_B$$

$$y_{2,C}F = y_{1,C} + Vr_C$$

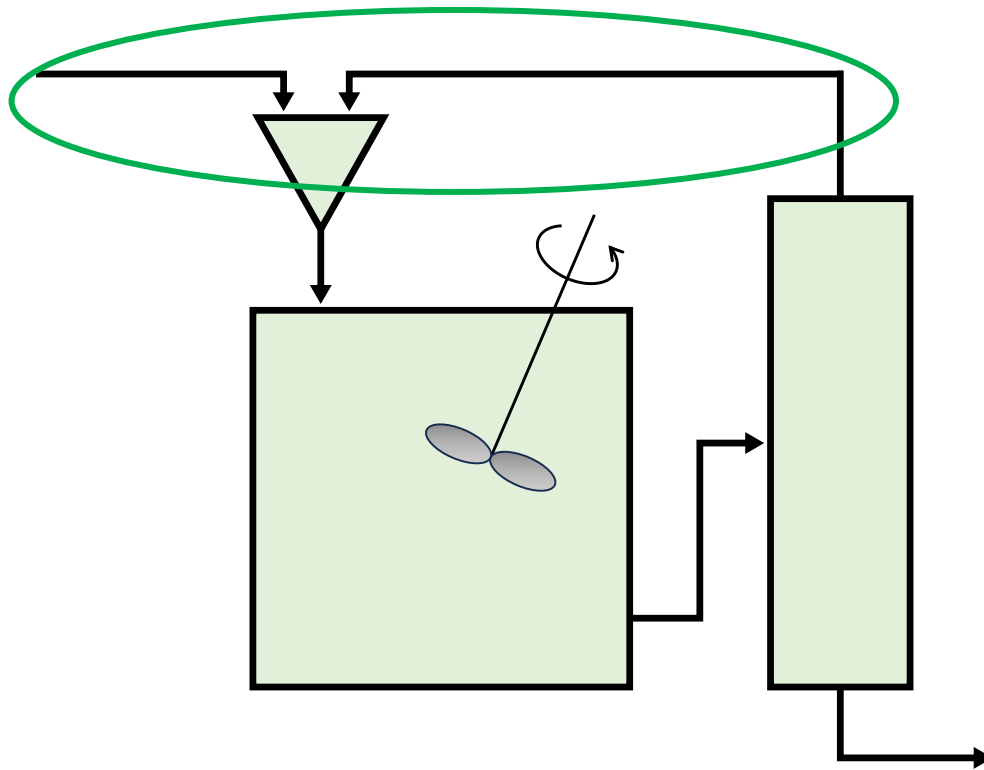
$$y_{3,A} = y_{1,A} - Vr_A$$

$$y_{4,B} + y_{4,C} = y_{2,B} + y_{2,C}$$

Modeling and Simulation Approaches

Causal/Sequential-Modular

Acausal/Equation-Oriented



$$y_{3,A} + y_{3,B} + y_{3,C} = 1$$

$$y_{3,B}F = y_{2,B} + Vr_B$$

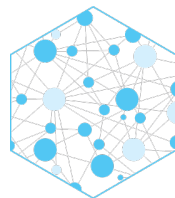
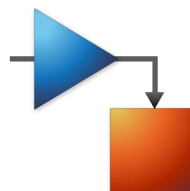
$$y_{3,C}F = y_{2,C} + Vr_C$$

$$y_{4,A} = y_{2,A} - Vr_A$$

$$y_{5,B} + y_{5,C} = y_{3,B} + y_{3,C}$$

$$y_{2,A} = y_{1,A} + y_{4,A}$$

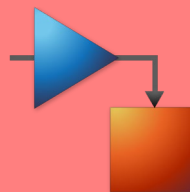
Available Software*



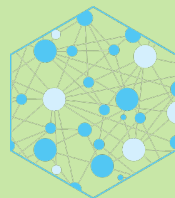
*Non-exhaustive list

Available Software*

Commercial



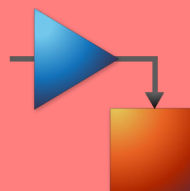
Open-source



*Non-exhaustive list

Available Software*

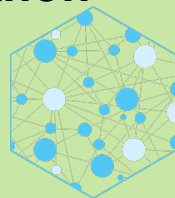
Commercial



Open-source



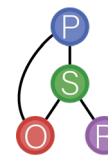
Python



Julia



*Non-exhaustive list

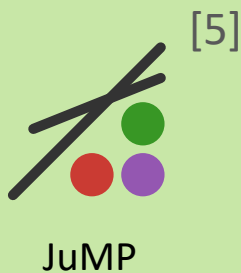


Why Julia?

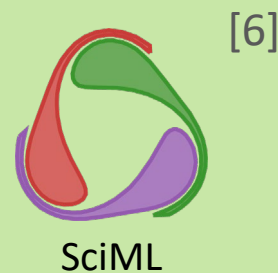


[4]

- Speed of C/Fortran
- Easy to use
- Strong scientific computing community



[5]

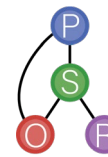


[6]

[4] Bezanson, J. et al. Julia: A Fresh Approach to Numerical Computing. *SIAM Review*. 59: 65–98 (2017).

[5] Lubin, M., Dowson, O., Garcia, J.D. et al. JuMP 1.0: recent improvements to a modeling language for mathematical optimization. *Math. Prog. Comp.* 15, 581–589 (2023).

[6] Dixit, V.K. and Rackauckas C. Optimization.jl: A Unified Optimization Package. (2023).

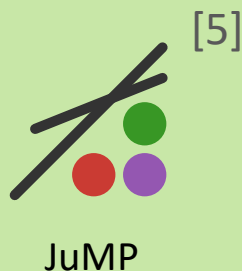


Why Julia?

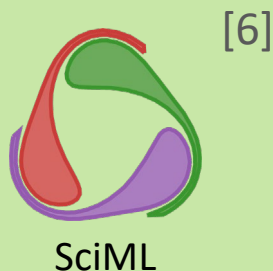


[4]

- Speed of C/Fortran
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[5]



[6]



[7]

- High-performance deterministic global solver
 - Dynamic optimization
 - User-defined functions
 - Semi-infinite programs
- Open-source

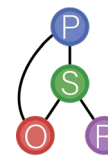


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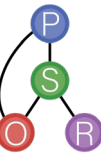
[6] Dixit, V.K. and Rackauckas C. Optimization.jl: A Unified Optimization Package. (2023).

[7] Wilhelm, M.E. and Stuber, M.D. EAGO.jl: easy advanced global optimization in Julia. *Optimization Methods and Software*. 37:2, 425-450 (2022).



ModelingToolkit.jl

- Open-source, acausal modeling framework in Julia
- Supports a broad range of system types
 - ODEs, SDEs, PDEs
 - Nonlinear systems
 - Optimization problems
- Automatically composes, transforms, and reduces models
 - Dimensionality reduction through algebraic simplification



Optimization in Julia

SciML

[6]



- 25+ libraries, 100+ solvers
- **No deterministic global optimization support**

JuMP

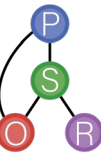
[5]



- Algebraic modeling language designed for mathematical optimization

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Optimization in Julia

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[6]



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EOptInterface
Abstraction layer



JuMP

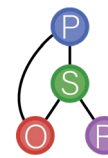
[5]



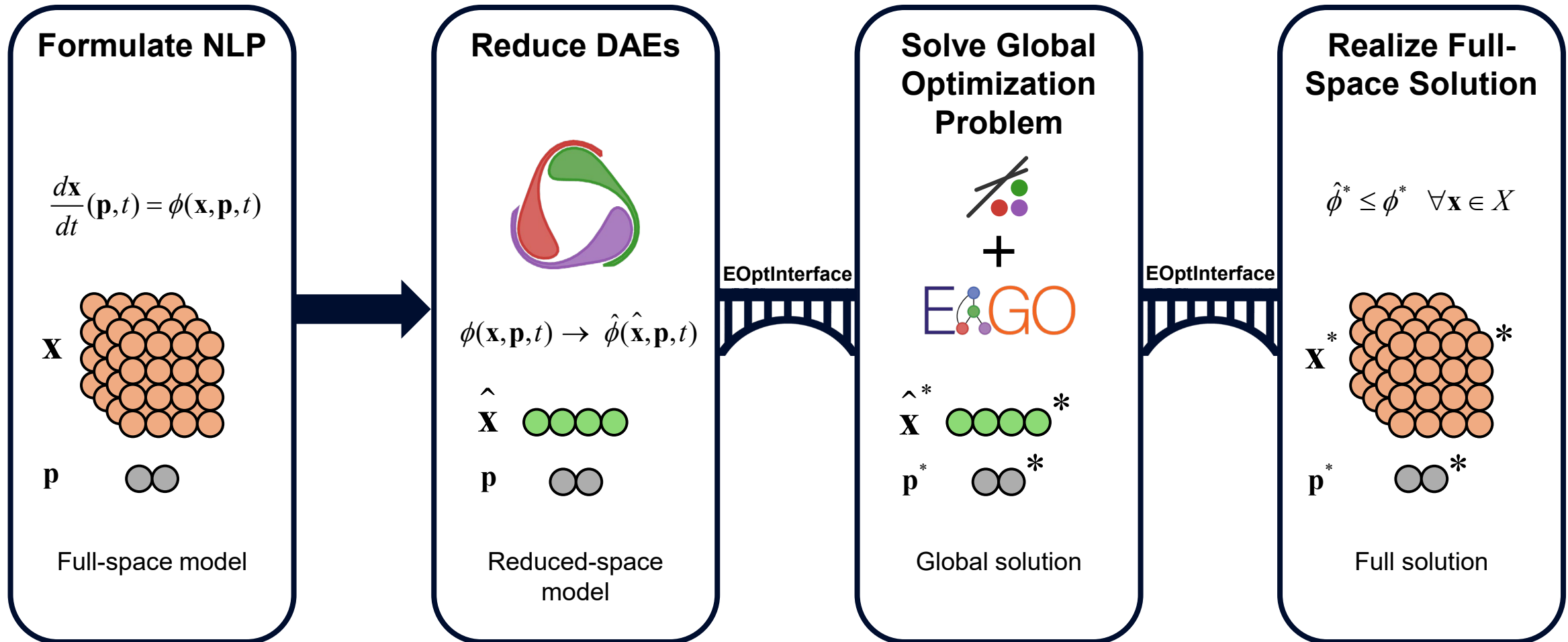
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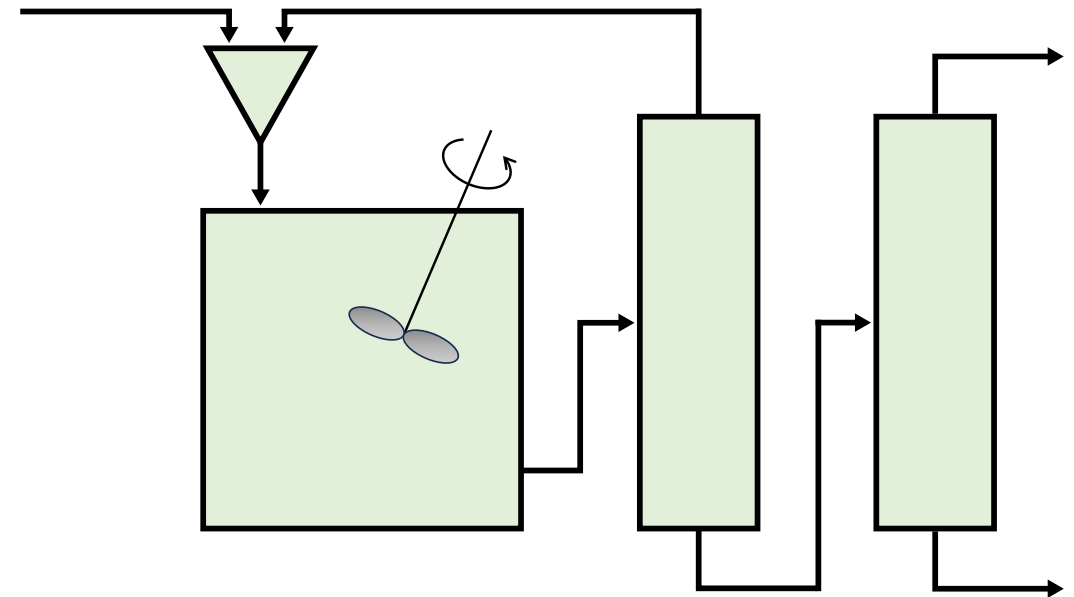
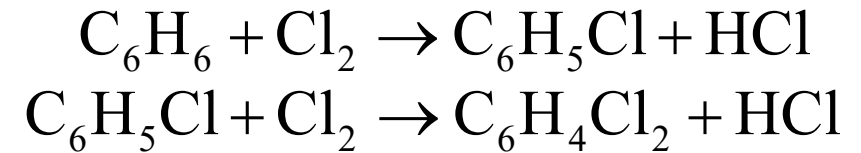


EOptInterface.jl



Steady-State Reactor Design Example

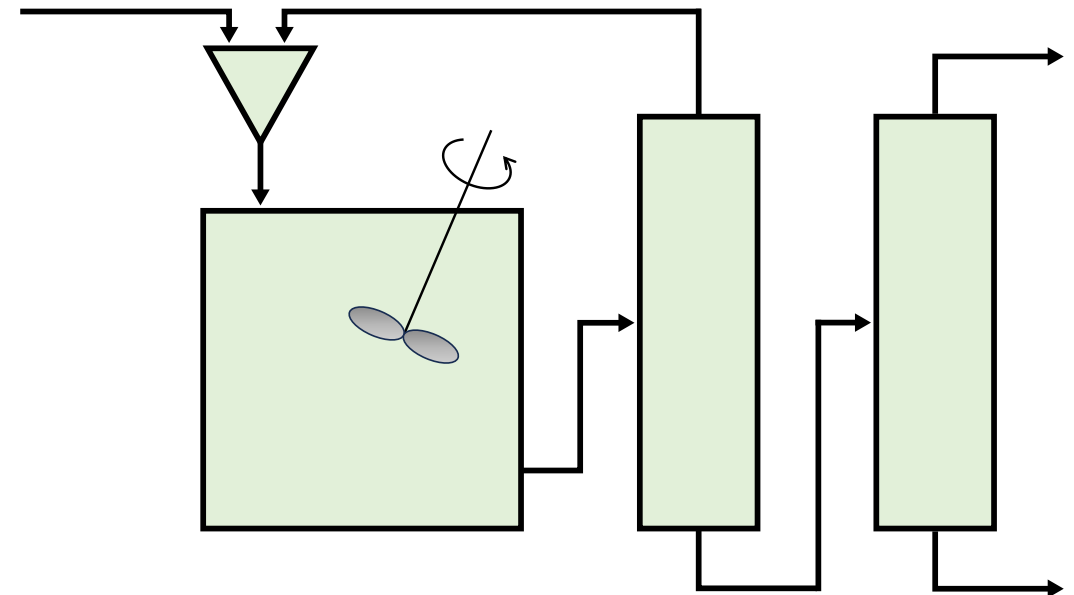
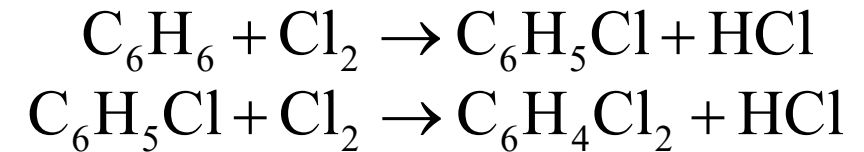
- Minimize total annualized costs
- Design variables:
 - Feed flowrate
 - Reactor volume



Steady-State Reactor Design Example

- Minimize total annualized costs
- Design variables:
 - Feed flowrate
 - Reactor volume

Model	Number of variables	Solve Time (s)
Full-space	50	202.0
Reduced-space	6	3.441



Kinetic Parameter Estimation Example

- Oxidation of cyclohexadienyl

$$\min_{\mathbf{p}} \phi(\mathbf{p}, t) = \sum_{i=0}^N (I_i^{calc} - I_i^{exp})^2$$

$$\text{s.t. } \mathbf{p} \in [\mathbf{p}^L, \mathbf{p}^U]$$

$$I_i^{calc} = x_{A,i} + \frac{2}{21}x_{B,i} + \frac{2}{21}x_{D,i}$$

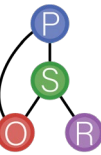
$$\frac{dx_A}{dt} = k_1 x_Z x_Y - c_{O_2} (k_{2f} + k_{3f}) x_A + \frac{k_{2f}}{K_2} x_D + \frac{k_{3f}}{K_3} x_B - k_5 x_A^2$$

$$\frac{dx_B}{dt} = c_{O_2} k_{3f} x_A - \left(\frac{k_{3f}}{K_3} + k_4 \right) x_B$$

$$\frac{dx_D}{dt} = c_{O_2} k_{2f} x_A - \frac{k_{2f}}{K_2} x_D$$

$$\frac{dx_Y}{dt} = -k_{1s} x_Z x_Y$$

$$\frac{dx_Z}{dt} = -k_1 x_Z x_Y$$

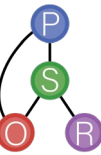


Kinetic Parameter Estimation Example

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$$\frac{dx_A}{dt} = k_1x_Zx_Y - c_{O_2}(k_{2f} + k_{3f})x_A + \frac{k_{2f}}{K_2}x_D + \frac{k_{3f}}{K_3}x_B - k_5x_A^2$$
$$\frac{dx_B}{dt} = c_{O_2}k_{3f}x_A - \left(\frac{k_{3f}}{K_3} + k_4\right)x_B$$
$$\frac{dx_D}{dt} = c_{O_2}k_{2f}x_A - \frac{k_{2f}}{K_2}x_D$$
$$\frac{dx_Y}{dt} = -k_{1s}x_Zx_Y$$
$$\frac{dx_Z}{dt} = -k_1x_Zx_Y$$



Kinetic Parameter Estimation Example

- Oxidation of cyclohexadienyl

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$$\text{s.t. } \mathbf{p} \in [\mathbf{p}^L, \mathbf{p}^U]$$

$$I_i^{calc} = x_{A,i} + \frac{2}{21}x_{B,i} + \frac{2}{21}x_{D,i}$$

$$\frac{dx_A}{dt} = k_1 x_Z x_Y - c_{O_2} (k_{2f} + k_{3f}) x_A + \frac{k_{2f}}{K_2} x_D + \frac{k_{3f}}{K_3} x_B - k_5 x_A^2$$

$$\frac{dx_B}{dt} = c_{O_2} k_{3f} x_A - \left(\frac{k_{3f}}{K_3} + k_4 \right) x_B$$

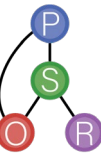
$$\frac{dx_D}{dt} = c_{O_2} k_{2f} x_A - \frac{k_{2f}}{K_2} x_D$$

$$\frac{dx_Y}{dt} = -k_{1s} x_Z x_Y$$

$$\frac{dx_Z}{dt} = -k_1 x_Z x_Y$$

```
@mtkmodel KineticParameterEstimation begin
  @parameters begin
    T = 273
    K_2 = 46*exp(6500/T-18)
    K_3 = 2*K_2
    k_1 = 53
    k_1s = k_1*1e-6
    k_5 = 1.2e-3
    c_O2 = 2e-3

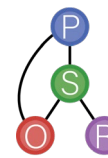
    k_2f
    k_3f
    k_4
  end
  @variables begin
    x_A(t) = 0.0
    x_B(t) = 0.0
    x_D(t) = 0.0
    x_Y(t) = 0.4
    x_Z(t) = 140.0
    I(t)
  end
  @equations begin
    D(x_A) ~ k_1*x_Z*x_Y - c_O2*(k_2f + k_3f)*x_A + k_2f/K_2*x_D + k_3f/K_3*x_B - k_5*x_A^2
    D(x_B) ~ c_O2*k_3f*x_A - (k_3f/K_3 + k_4)*x_B
    D(x_D) ~ c_O2*k_2f*x_A - k_2f/K_2*x_D
    D(x_Y) ~ -k_1s*x_Z*x_Y
    D(x_Z) ~ -k_1*x_Z*x_Y
    I ~ x_A + 2/21*x_B + 2/21*x_D
  end
end
```



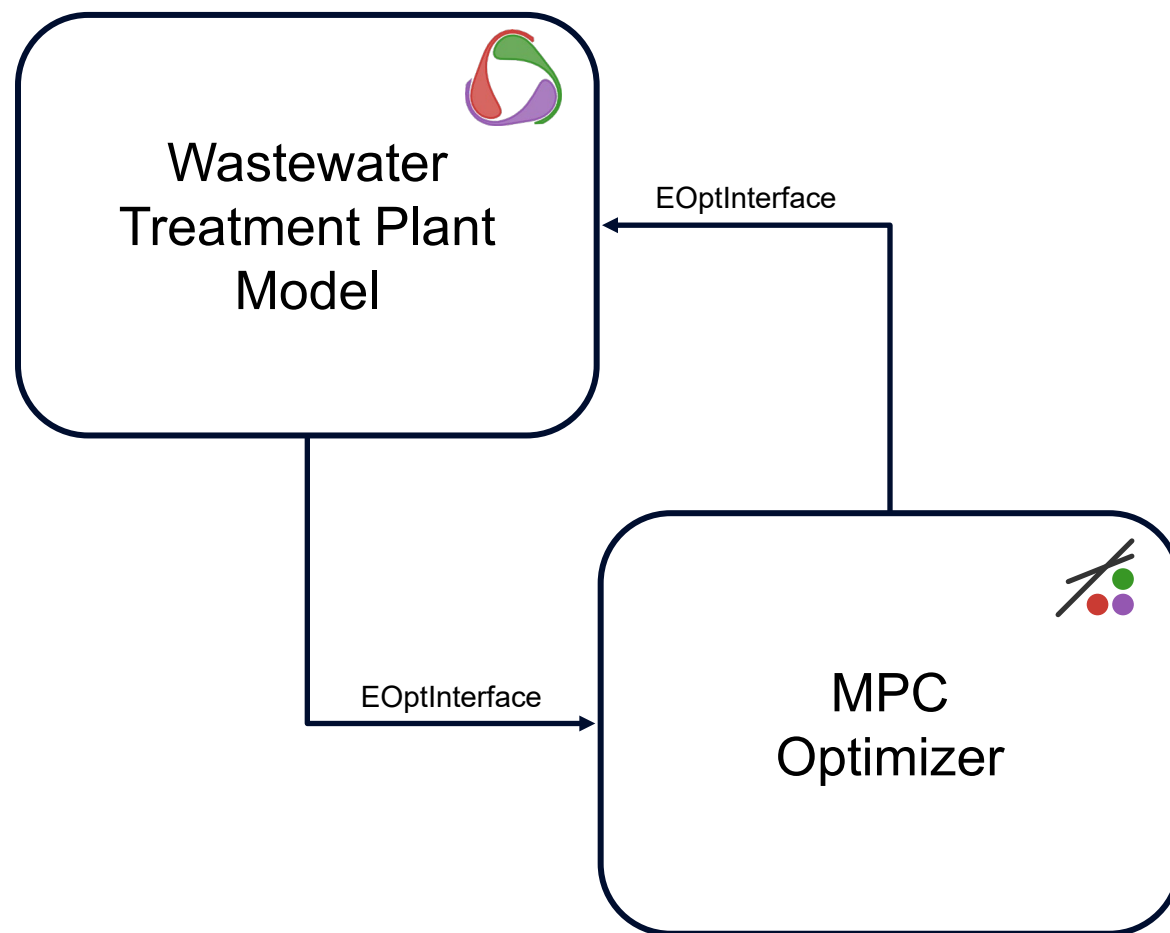
Kinetic Parameter Estimation Example

- Oxidation of cyclohexadienyl

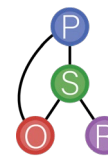
Integration Method	Objective Value	Solve Time (s)
Explicit	9622.8	0.1072
Implicit	16796.0	0.1006



Nonlinear Model Predictive Control

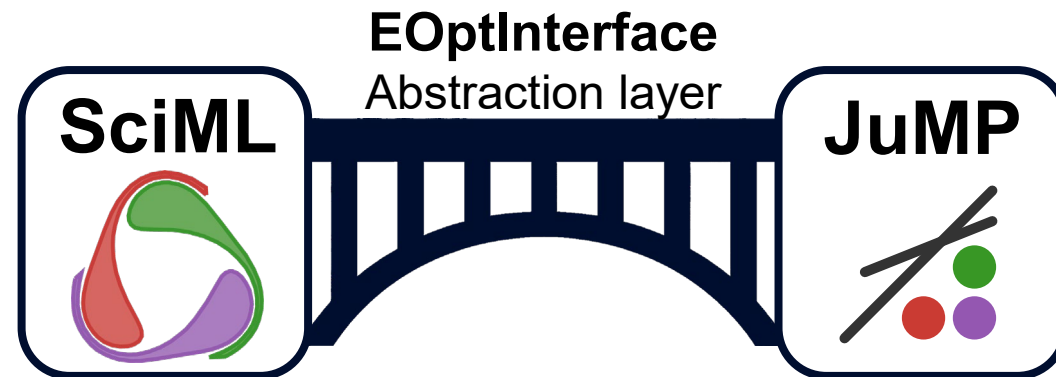


124e Improving
Operations of
Wastewater Treatment
Plants Using Economic
MPC



Conclusion

- Deterministic global optimization tools are necessary for complex engineering models
- EOptInterface.jl
 - Seamlessly integrates modeling and simulation with formal optimization
 - Contains multiple discretization techniques for ODEs
 - You can use your favorite solver



Acknowledgements

Members of the Process Systems and Operations Research Laboratory at the University of Connecticut (<https://www.psor.uconn.edu>)



Pratt & Whitney

Institute for Advanced Systems Engineering

UNIVERSITY OF CONNECTICUT



Funding:

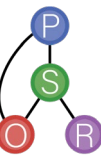
Department of Energy, Award No.: DE-EE0010991

National Science Foundation, Award No.: 2051084

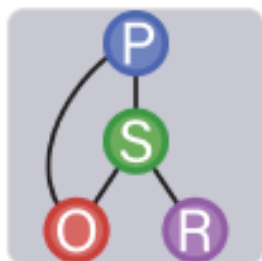
Pratt & Whitney Endowed Professorship

Any opinions, findings, and conclusions or recommendations expressed in this material are those of the authors and do not necessarily reflect the views of the National Science Foundation or the United States Government.

AIChE Annual Meeting 2025



Questions?



Process Systems and Operations Research Laboratory

The PSOR Laboratory at UConn develops numerical analysis methods and software for process systems engineering applications.

22 followers

University of Connecticut, Storrs, CT, ...

<https://psor.uconn.edu>

stuber@uconn.edu

<https://psor.uconn.edu>



<https://github.com/PSORLab>

